

Characterization of Oxy-combustion Impacts in Existing Coal-fired Boilers

**Bradley Adams, Andrew Fry¹,
Brydger Van Otten, Tim Shurtz**



*For Energy and
Environmental
Solutions*

REACTION ENGINEERING INTERNATIONAL

77 West 200 South, Suite 210 Salt Lake City, UT 84101
TEL: +1 (801) 364-6925 FAX: +1 (801) 364-6977
<http://www.reaction-eng.com>

¹ *University of Utah*



**2013 NETL CO₂ Capture
Technology Meeting
July 8-11, 2013**

Presentation Outline

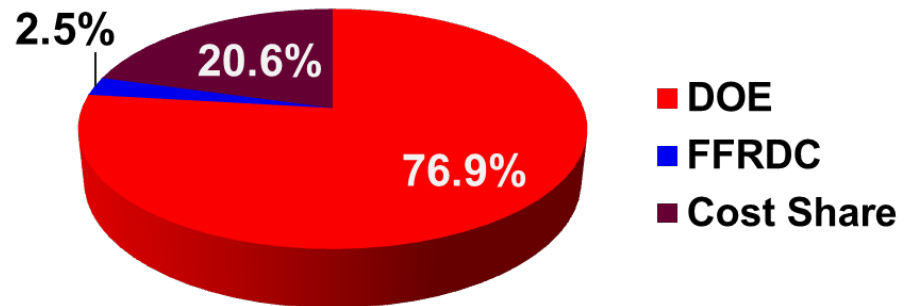
- **Project Overview**
- **Summarize Previous Work**
- **Introduce Current Work**
- **Preliminary Testing Results**
 - **Bench-scale Mercury Measurements**
 - **Pilot-scale Mercury Measurements**
 - **Pilot-scale Corrosion Measurements**
- **Project Status Summary**



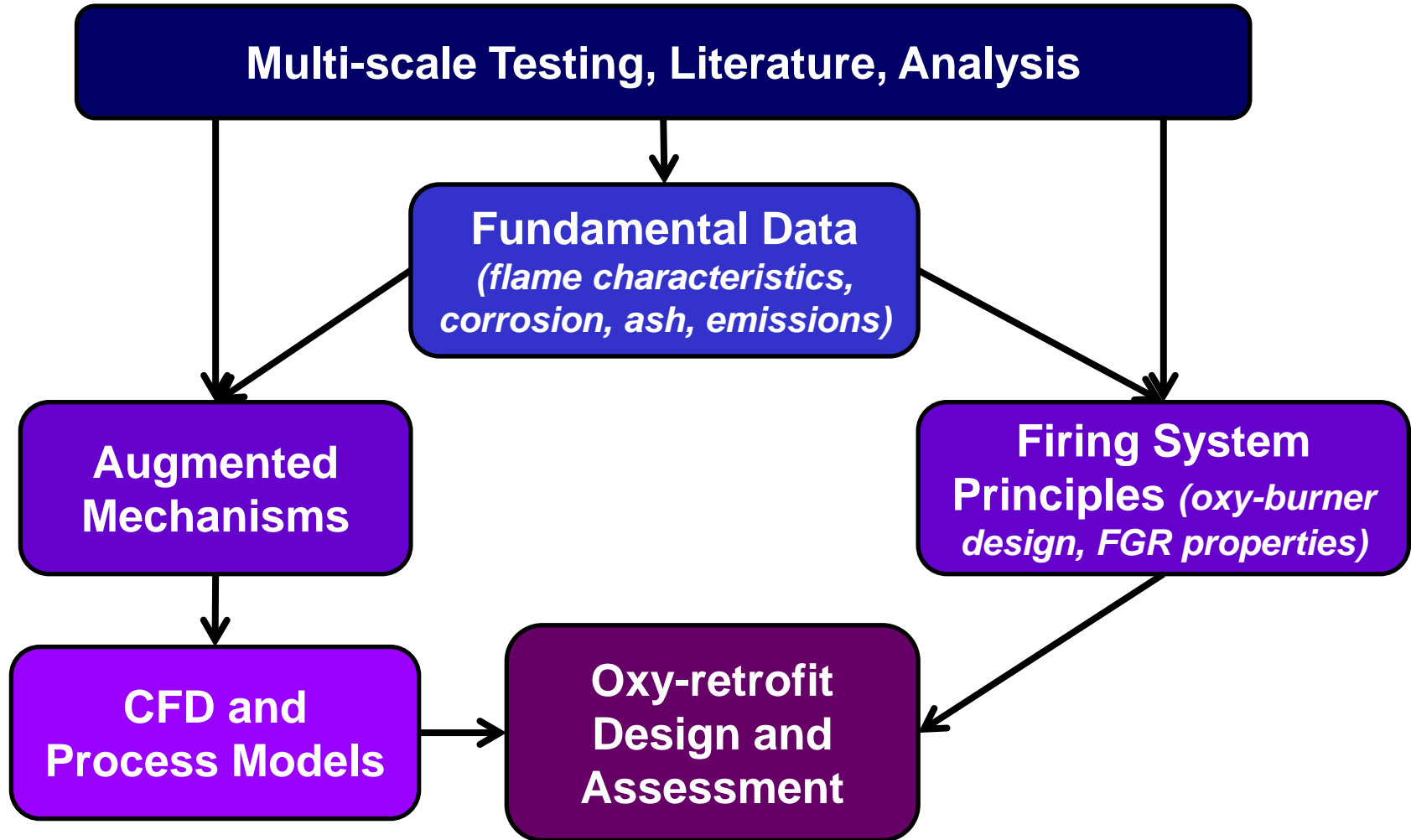
Project Overview

- **Objective:** *Characterize and predict performance and operational impacts of oxy-combustion retrofit designs on existing coal-fired boilers*
- **Schedule:** 10/1/08 – 9/30/13 (includes 1-yr extension)
- **Program Managers:** Timothy Fout, Andrew Jones
- **Budget:** \$4M total

Funding Distribution (\$4M total)



Project Approach



Project Team

Team Members	Project Role
REI	<i>program management, testing oversight, mechanism development, simulations</i>
University of Utah	<i>laboratory and pilot-scale testing, mechanism development</i>
Siemens Energy	<i>burner technology, firing system design</i>
Praxair	<i>oxygen and CO₂ supply</i>
Brigham Young Univ.	<i>soot measurements</i>
Corrosion Management	<i>corrosion tests, mechanism development</i>
Sandia National Labs	<i>bench-scale testing, mechanism development</i>
Vattenfall AB	<i>mechanism development, validation data</i>
DTE, PacifiCorp, Praxair, Southern Company, Vattenfall	<i>Advisory Panel provides industrial perspective on R&D needs, retrofit requirements and constraints, suggested assessment studies</i>



Previous Work

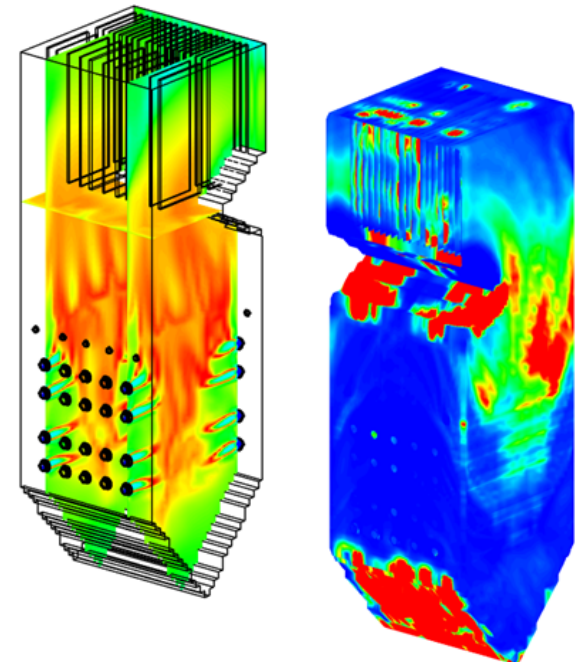
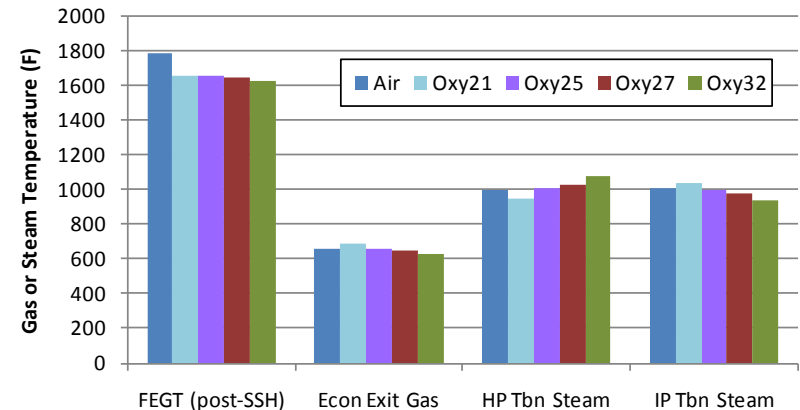
- **Testing at bench- and pilot-scales**
 - **Ignition & flame attachment**
 - **Char oxidation**
 - **NO_x, SO_x, Hg**
 - **Soot**
 - **Heat flux profiles**
 - **Fine particulates / ash aerosols**
 - **Ash chemistry**
 - **Waterwall and superheat tube corrosion**
- **Impacts of oxy-coal burner design and recycle gas properties**



Previous Work

- **Mechanism refinement**
 - Slagging / fouling
 - Char oxidation
 - Soot
 - Gas radiation
 - Corrosion
- **Two full-scale oxy-retrofit assessments**
 - Firing-system design
 - CFD & process modeling of combustion, heat transfer, steam properties, deposition, corrosion, emissions
- **Technology Transfer - 45 conference presentations, posters, journal articles and book chapters (to date)**

Gas and Steam Temperatures



Previous Work – Key Results

- **Firing System and Oxy-combustion Burner**
 - Oxy-combustion flame can be designed similar to air-fired flame
 - Oxygen and FGR provide additional degree of freedom
 - ~25-26% oxygen gives reasonable match to air-fired heat transfer
 - FGR properties impact overall heat transfer
 - Reduced flue gas flow may require convective pass adjustments
- **Operational Impacts**
 - Slagging behavior and ash properties similar to air-firing
 - Corrosion similar unless recycle creates high SO₂ and H₂O levels
- **Emissions**
 - Lower NO_x, potentially higher SO₂, soot more dependent on burner SR, enhanced char oxidation (lower LOI)
- **No combustion show-stoppers for retrofit**



Current Work (1-yr extension)

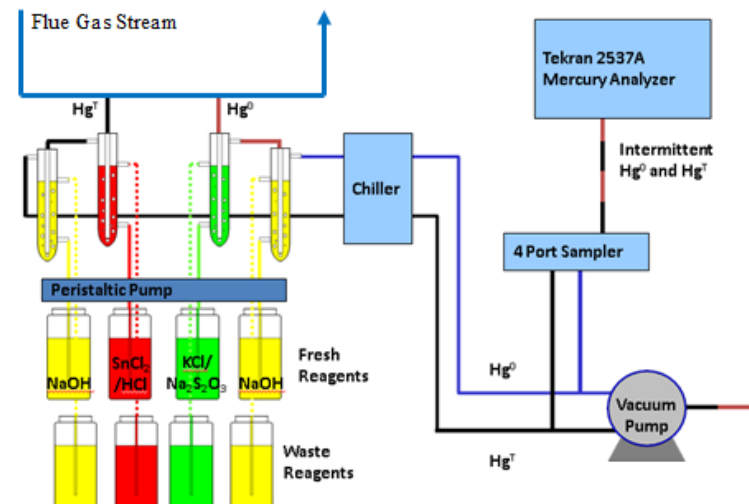
Motivation: Mercury may amalgamate with aluminum surfaces in oxy-combustion flue gas processing units

- 1) Determine accuracy of different mercury measurement methods for air and oxy-combustion firing (bench-scale)**
- 2) Measure impact of oxy-combustion on performance of mercury control technologies (pilot-scale)**
 - Bromine boiler additive**
 - Activated carbon injection**
- 3) Measure corrosion impacts of bromine addition under air and oxy-firing conditions (pilot-scale)**
- 4) Model mercury emissions and control in oxy-retrofit plants**



Bench-Scale Measurements

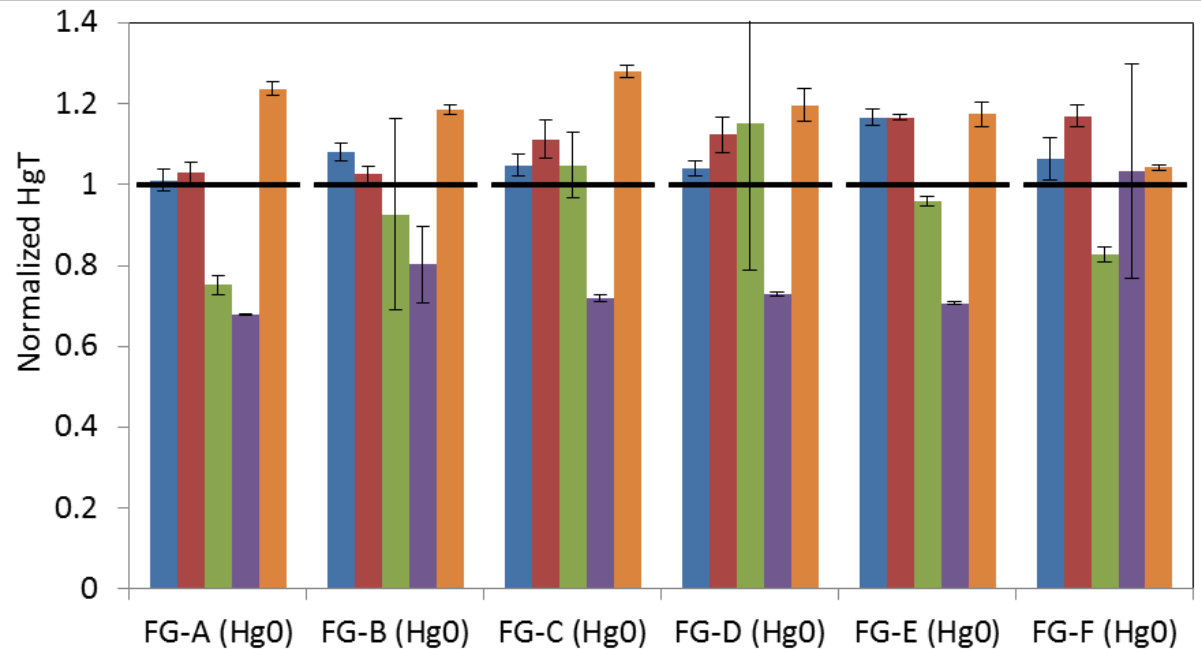
- Objective: Assess potential for mercury measurement bias under different flue gas environment
 - Previous studies have shown possibility for CO₂ absorption in highly concentrated NaOH solution in measurement conditioning systems
- Approach
 - Simulate flue gas with Hg calibration gas generator
 - Assess three Hg measurement techniques
 - Tekran CEM with wet conditioning system (two NaOH solutions)
 - Modified method 30B sorbent traps
 - OL CEM w/ thermo-catalytic conversion
 - Compare elemental and oxidized Hg measurements for different methods



Bench-scale Summary (PRB coal)

- Wet conditioning system and OL CEM gave reasonable results
- Speciating carbon traps gave low mercury measurements
- Results with “B” solutions (highest NaOH concentrations) increased slightly with higher CO₂ concentration, but similar to data scatter

Overall, no clear Hg measurement bias in high CO₂ environments was noted



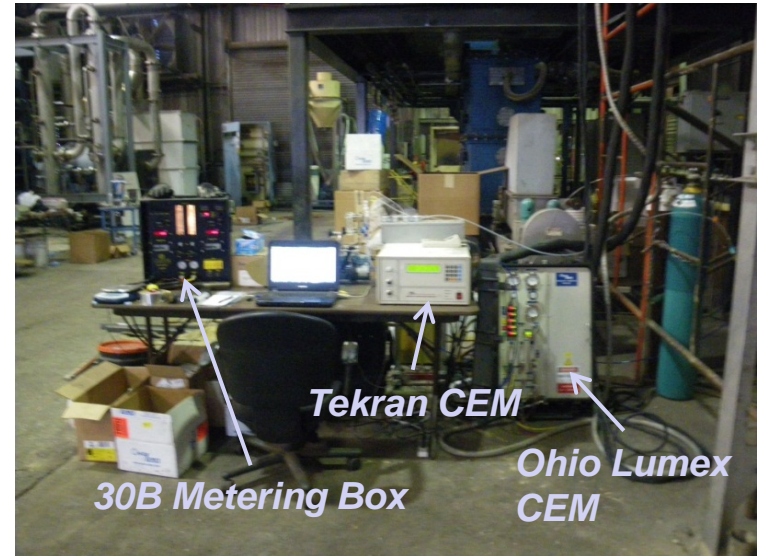
■ A solutions ■ B solutions ■ 30B trap
■ Spec trap ■ OL CEM

	N2	O2	CO2	H2O	SO2	NO
A	94	0	0	6	0	0
B	89	5	0	6	0	0
C	77	5	12	6	0	0
D	64	5	25	6	0	0
E	9	5	80	6	0	0
F	9	5	80	6	420	200



Pilot-Scale Measurements

- **Objective - Measure impact of oxy-combustion on performance of mercury control technologies**
- **Approach**
 - **L1500 pilot-scale furnace**
 - **PRB and bituminous coals**
 - **Air and oxy-firing**
 - **Two Hg control technologies**
 - **Bromine boiler additive (CaBr_2)**
 - **Activated carbon injection**
 - **Hg measured before and after baghouse**
 - **Three different Hg measurement techniques**
 - **Testing in May and June 2013**



L1500 Operating Conditions (PRB coal)

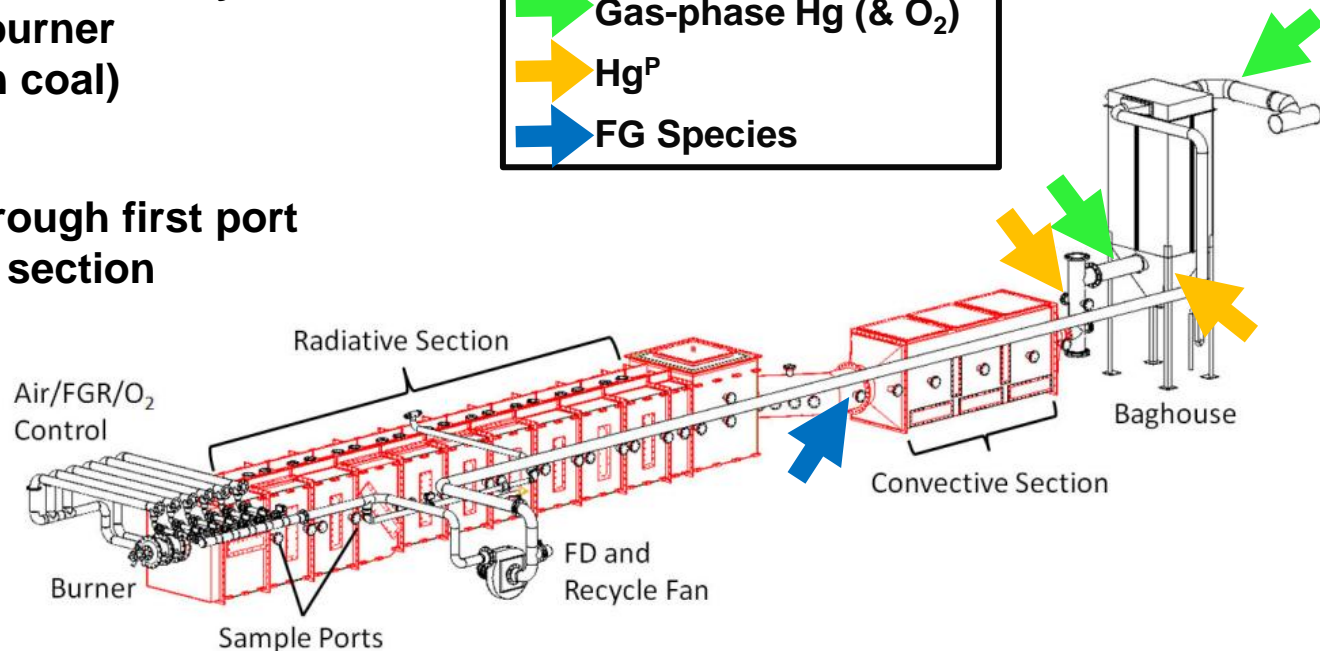
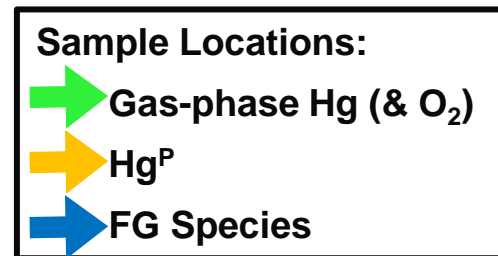
	Firing Rate (kW)	O ₂ (%, dry)	CO ₂ (%, dry)	BH inlet (F)	BH outlet (F)
Air-Fired	780-860	4.0	14	380	250
Oxy-Fired	780	3.5	83	300	140

Br addition:

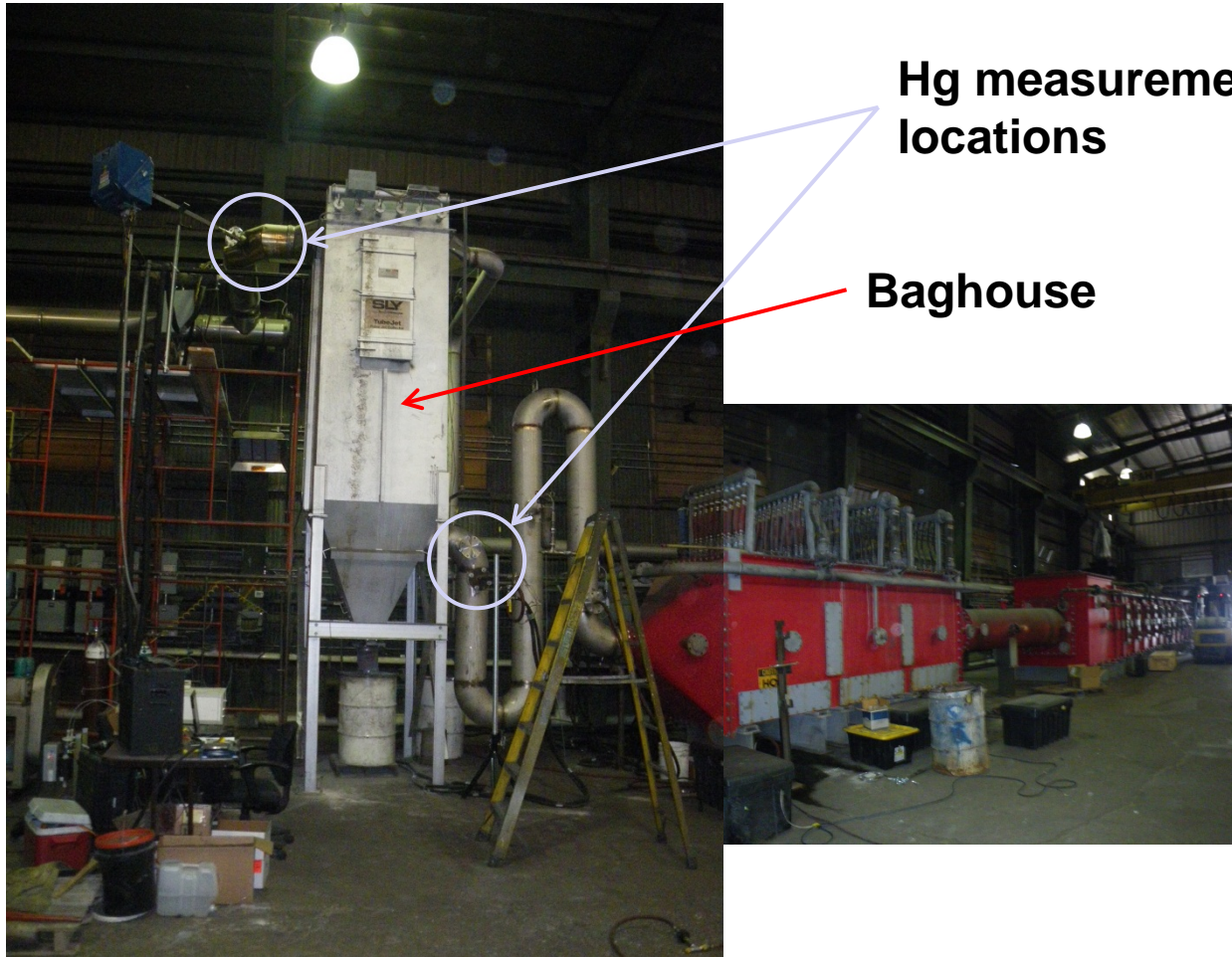
Solid CaBr₂ injected immediately
before coal entered burner
(~8-75 ppm Br wet on coal)

ACI:

Darco Hg injected through first port
following convective section
(~0.5-10 lb/MMacf)

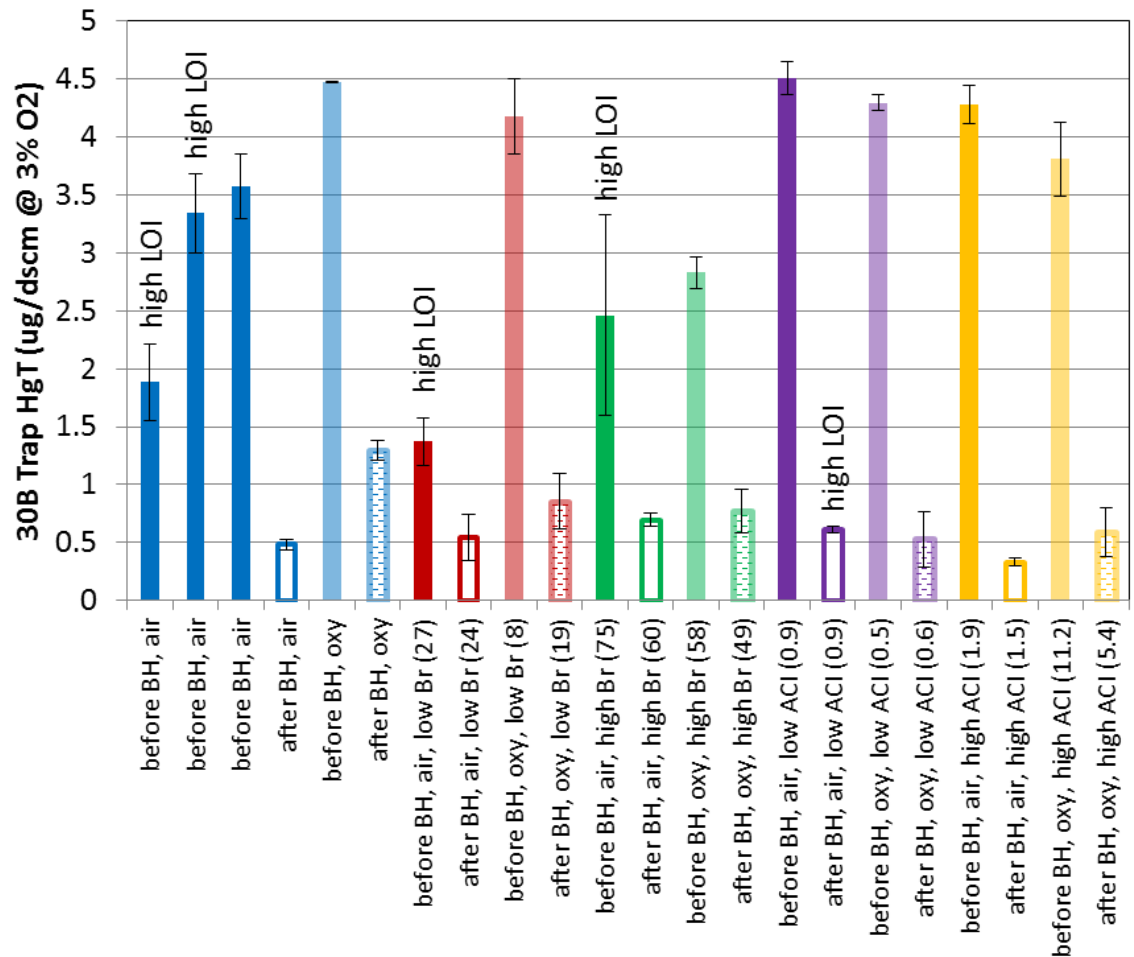


L1500 Mercury Testing Setup



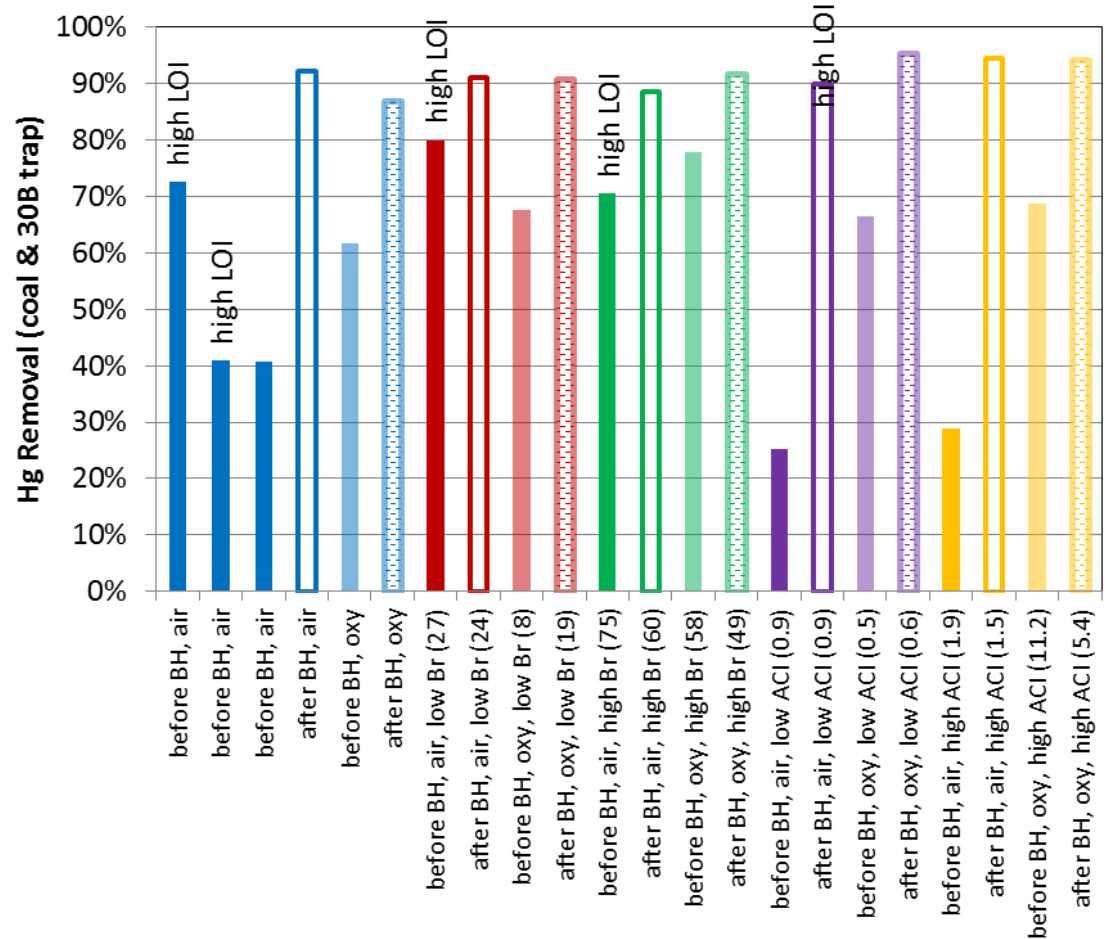
Mercury Emissions (PRB Coal)

- Total Hg levels lower after the baghouse
- Oxy-firing increased emission levels
- Effect of CaBr_2 & ACI similar for air vs oxy



Mercury Removal (PRB coal)

- Mercury removal higher after baghouse
- After BH, air and oxy removal levels comparable
- Addition of CaBr_2 or ACI increased removal
 - Br addition increased removal before BH
 - ACI increased removal across BH



Preliminary Mercury Summary

(PRB coal)

- Mercury mass balance poor for many conditions, likely due to unrepresentative ash samples (dropout)
- The three measurement methods generally agreed with the exception of the OL CEM values before the baghouse
 - Uncharacteristically low levels, particles on dilution probe?
- Oxy-firing tended to increase Hg emission and oxidation
 - Flue gas recycle increases Hg and halogen concentrations
- Mercury emissions decreased with addition of CaBr_2 or ACI
- No significant difference in additive performance was seen between air- and oxy-firing



Pilot-scale Corrosion Measurements

Objective:

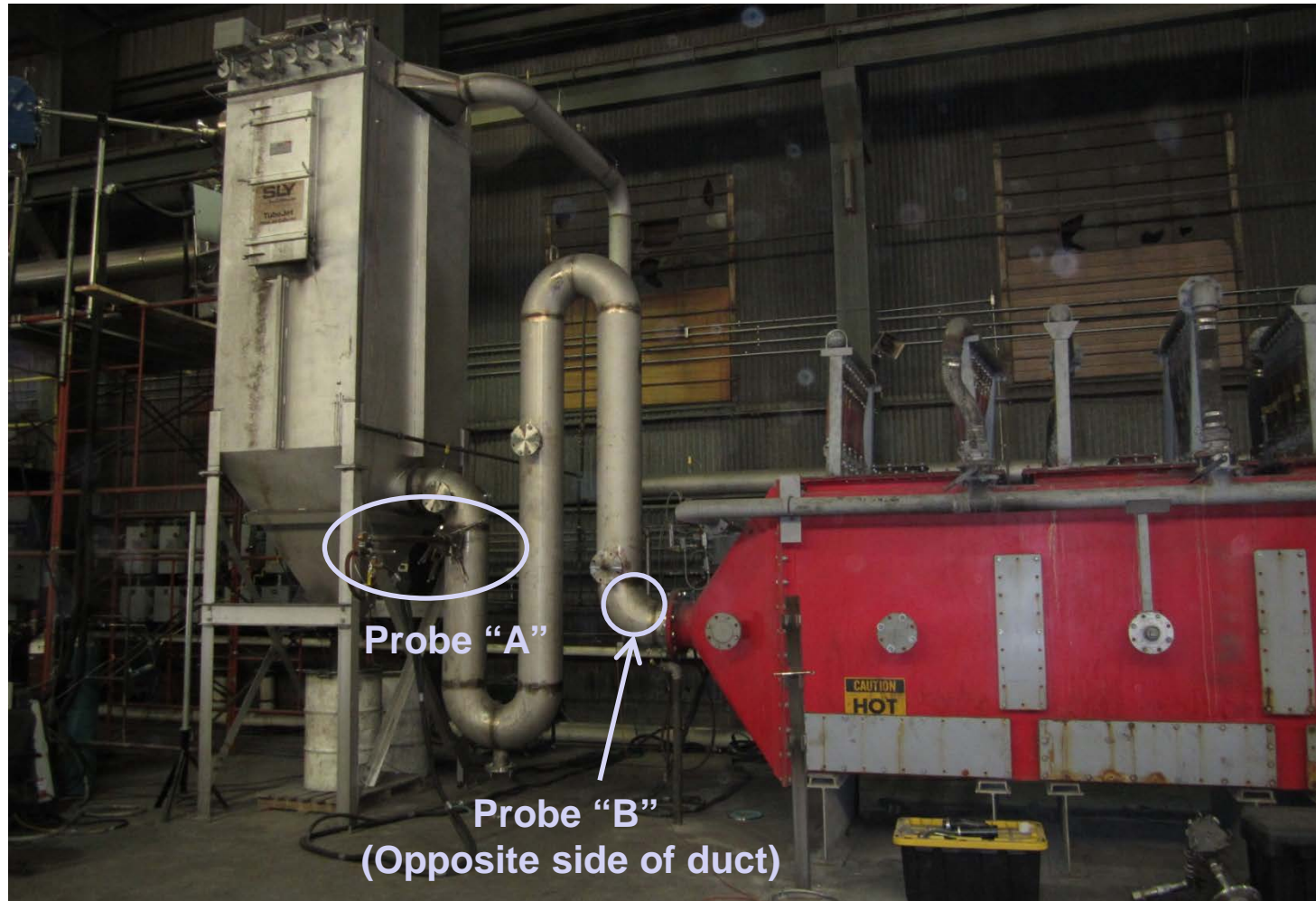
- **Measure changes in corrosion rates at temperatures representative of an air heater,**
- **In the presence of various mercury control additives (baseline, bromine, activated carbon),**
- **Under both air-fired and oxy-fired conditions**

Method:

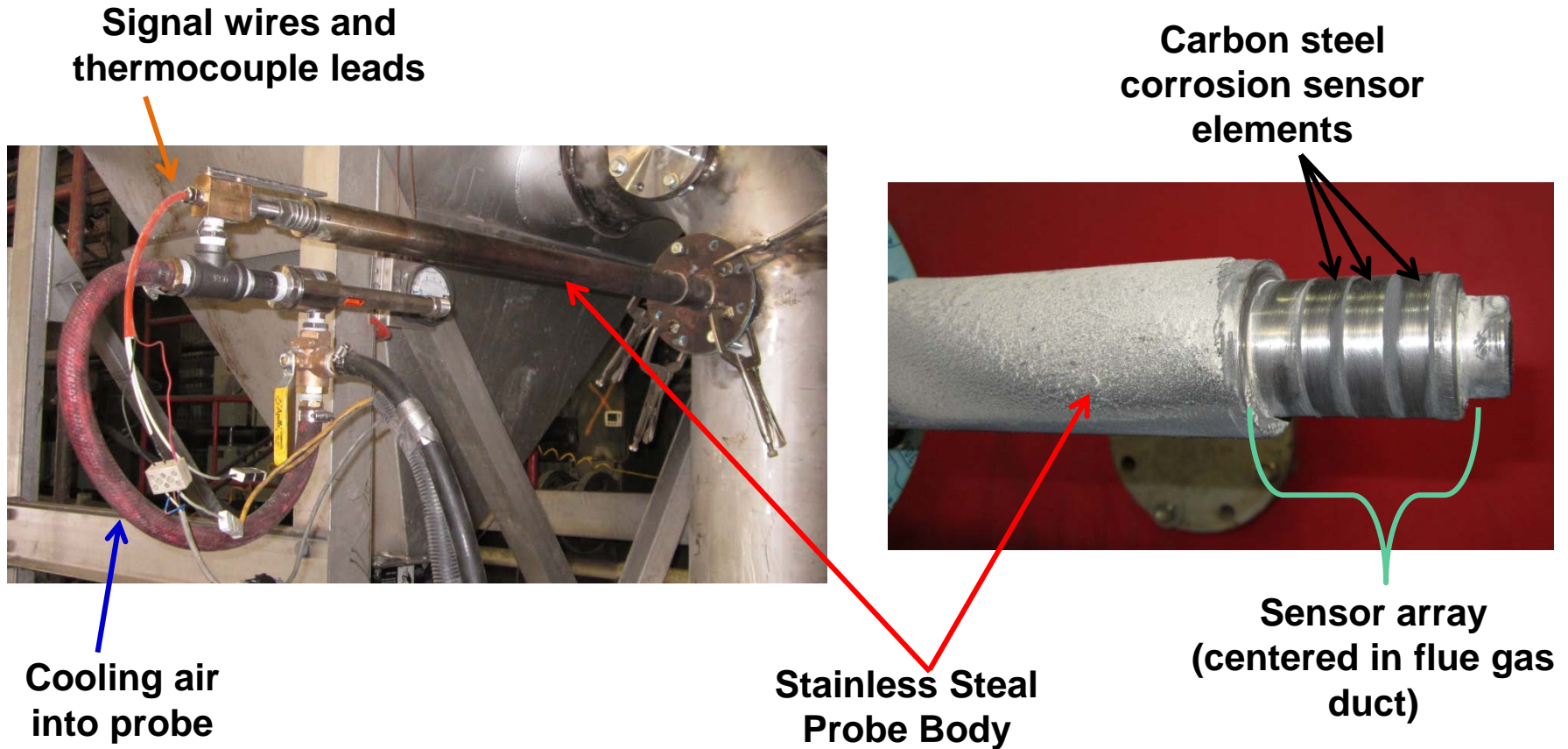
- **Use air cooled corrosion probes positioned in the flue gas just upstream of the baghouse**
- **Vary probe cooling to alter element surface temperature to be representative of air heater temperatures**
- **Only bituminous coal results shown**



Corrosion Probe Placement



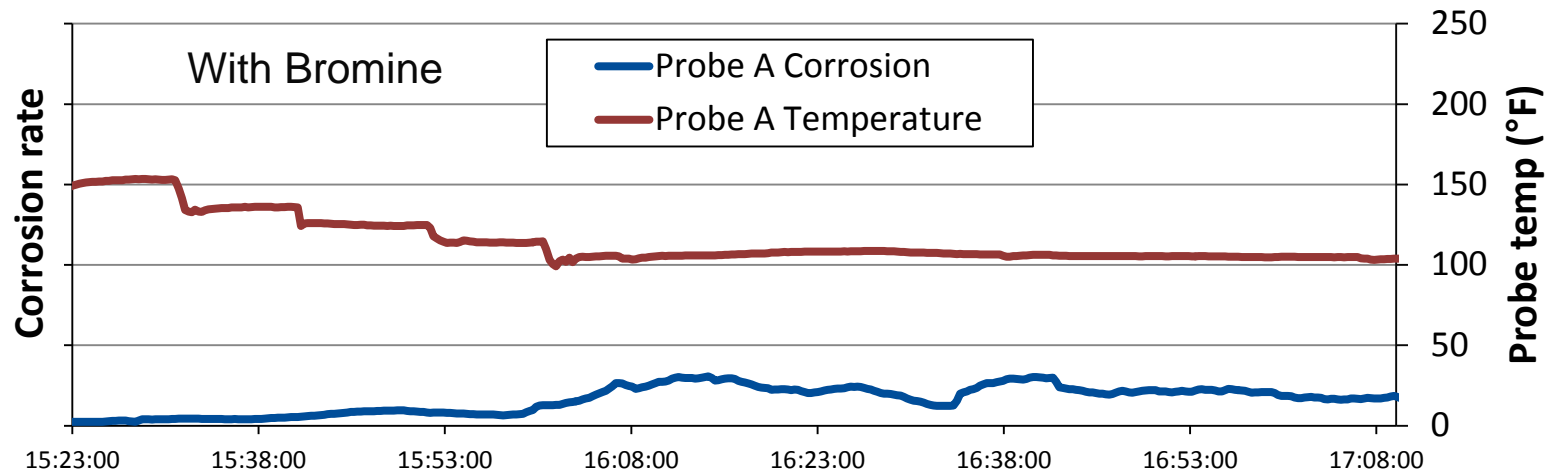
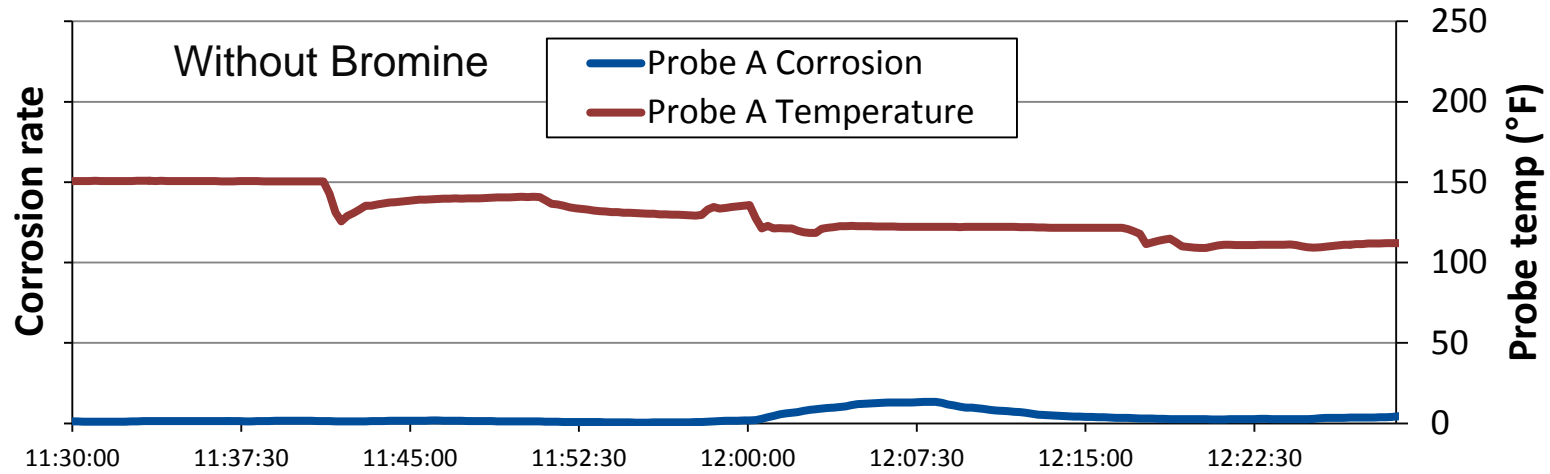
ECN Corrosion Probes



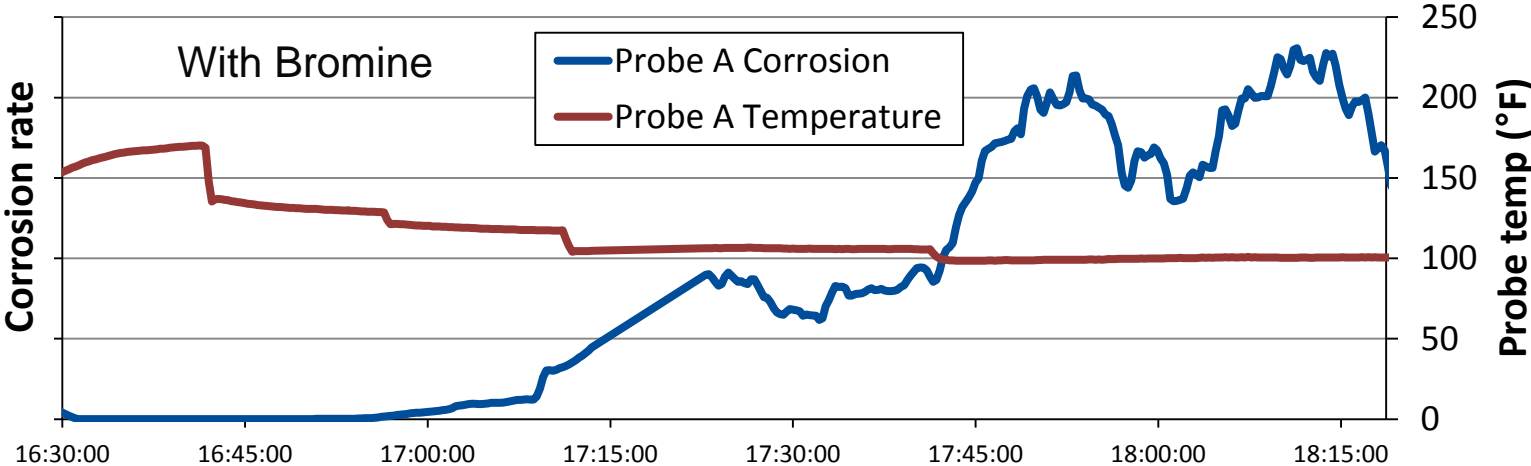
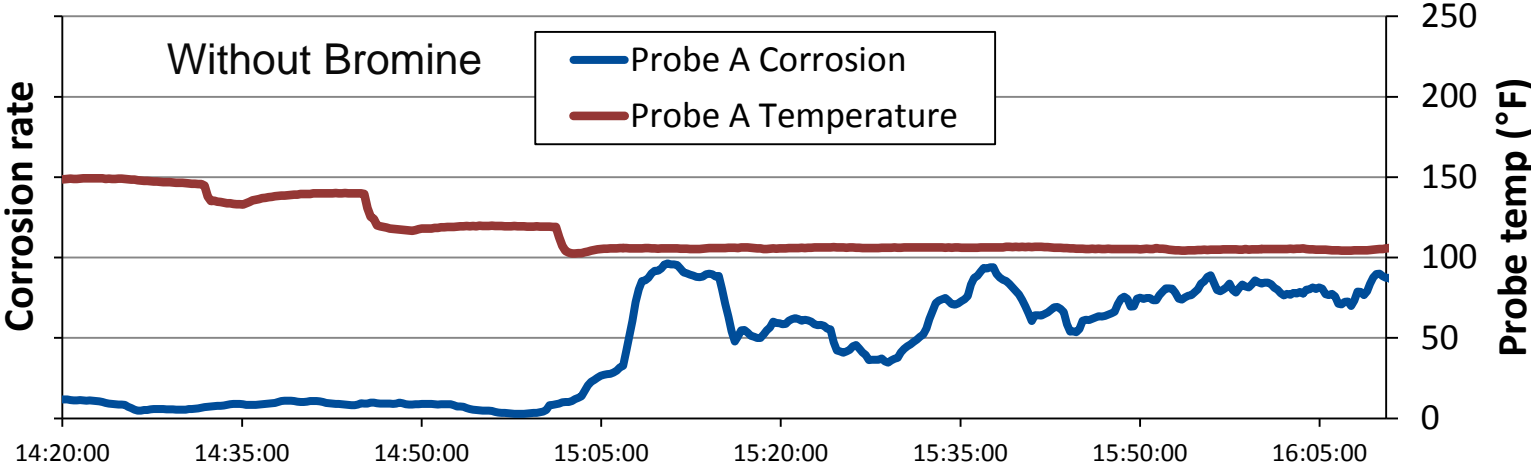
Sensor surface temperatures were varied between ~350 °F and ~100 °F



Smoothed Corrosion Rates (air-fired) (bituminous coal)



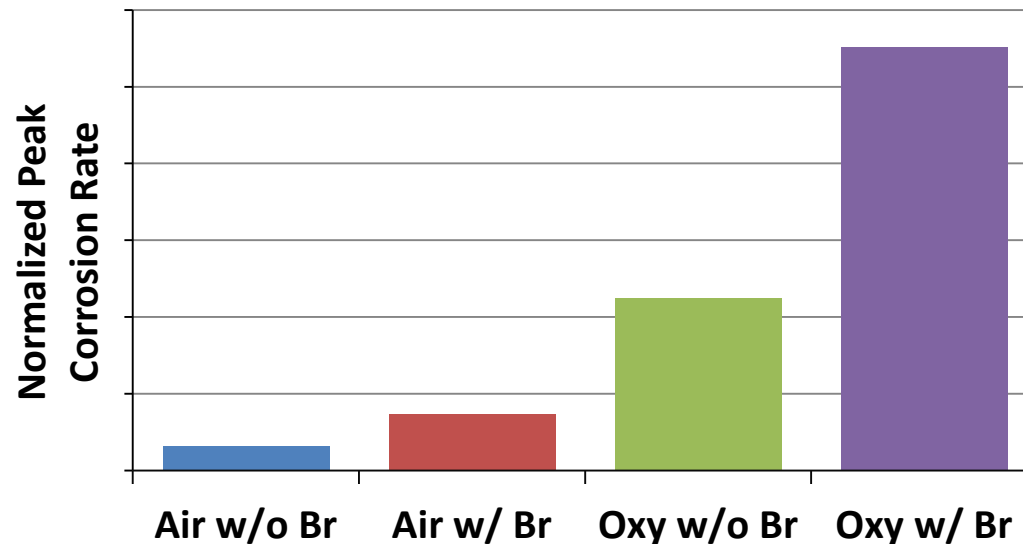
Smoothed Corrosion Rates (oxy-fired) (bituminous coal)



Preliminary Corrosion Summary

(bituminous coal)

- Corrosion rates increased with bromine addition
- Corrosion rates increased with oxy-combustion
- Suspect dew point corrosion for sulfur (SO_3) and bromine
 - Rates dependent on flue gas concentrations and moisture level (both higher with oxy-combustion)
 - Different mechanism than high-temperature corrosion



Project Status

- **Previously completed testing and modeling work on oxy-combustion flame characteristics, operational impacts, firing system design and full-scale retrofit evaluations**
- **Completed bench-scale Hg measurement evaluation**
- **Completed pilot-scale air and oxy-firing tests:**
 - **Hg emissions and control technologies**
 - **Low-temperature corrosion**
- **Next tasks:**
 - **Hg modeling of full-scale oxy-retrofit unit (9/30/13)**
 - **Complete final report and project close-out**



Acknowledgment

This material is based upon work supported by the Department of Energy under Award Number DE-NT0005288; Andrew Jones, Program Manager.



Disclaimer

This material is based upon work supported by the Department of Energy under Award Number DE-NT0005288. Project Manager is Andrew Jones. This report was prepared as an account of work sponsored by an agency of the United States Government. Neither the United States Government nor any agency thereof, nor any of their employees, makes any warranty, express or implied, or assumes any legal liability or responsibility for the accuracy, completeness, or usefulness of any information, apparatus, product, or process disclosed, or represents that its use would not infringe privately owned rights. Reference herein to any specific commercial product, process, or service by trade name, trademark, manufacturer, or otherwise does not necessarily constitute or imply its endorsement, recommendation, or favoring by the United States Government or any agency thereof. The views and opinions of authors expressed herein do not necessarily state or reflect those of the United States Government or any agency thereof.

